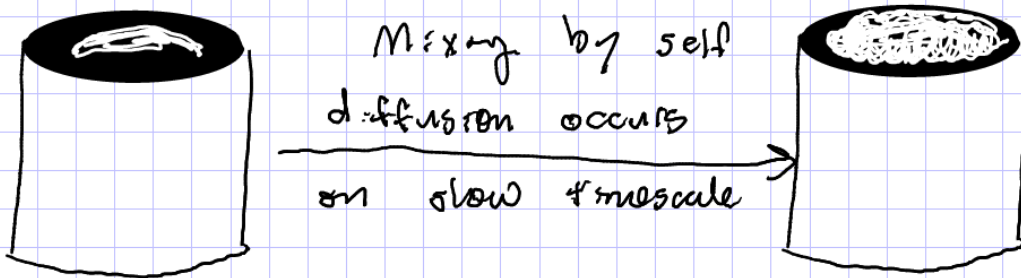


I Introduction to turbulence and (K4)

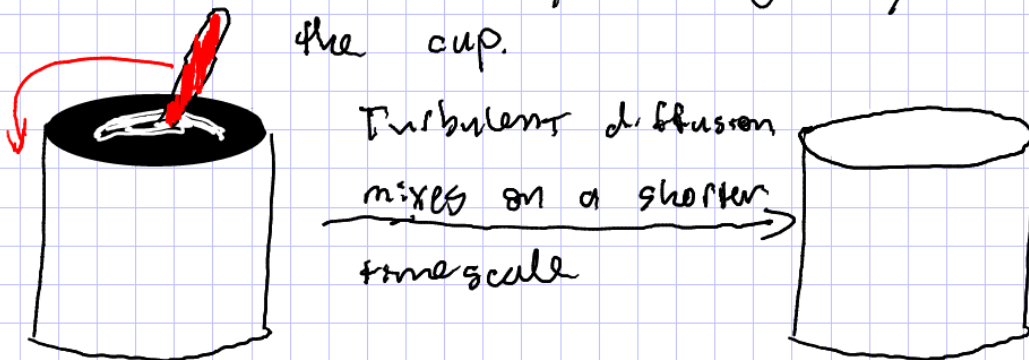
Turbulence is a chaotic flow regime characterized by diffusivity, rotationality, and dissipation.

Cartoon picture of Turbulence

Mixing of cream (tracer) into coffee



Instead, we stir. Thereby injecting energy at the scale of the cup.



Equations of Hydrodynamic Turbulence (Euler Eqs)

1) Incompressibility, $\rho = \text{const} \Rightarrow \nabla \cdot \vec{u} = 0$

2) Navier-Stokes (NS)

$$\frac{\partial \vec{u}}{\partial t} + \underbrace{\vec{u} \cdot \nabla \vec{u}}_{\text{Convection (Nonlinear term)}} = -\nabla \left(\frac{p}{\rho} \right) + \underbrace{\nu \nabla^2 \vec{u}}_{\text{viscosity}} + \underbrace{\vec{f}}_{\text{External forcing}}$$

↑
↑
↑
↑

3) Energy: $\frac{\partial E}{\partial t} + \nabla \cdot [\vec{u}(E+p)] = 0$; $E = \frac{1}{2} \rho u^2 + \rho e$, $e = \text{internal energy}$

Aside: when can we assume incompressibility?

page 1) $\Delta P / \rho \ll 1$: Adiabatic change in $\Delta p \Rightarrow \Delta p = (\partial p / \partial \rho)_s \Delta \rho$

Bernoulli's eqn $\Rightarrow \Delta p \sim \rho u^2$ and $(\partial p / \partial \rho)_s \equiv c_s^2 \equiv \gamma p / \rho$ Ideal gas

$\therefore \Delta p / \rho \ll 1 \Rightarrow u / c_s = Ma \ll 1$ $Ma \equiv$ Mach number

a) $\partial^2 / \partial t^2 \ll \rho \nabla \cdot \ddot{u}$: $\frac{\partial^2 p}{\partial t^2} \sim \frac{\Delta p}{t^2} \sim \frac{\rho u^2}{t c_s^2}$; $\rho \nabla \cdot \ddot{u} \sim \rho u / l$

$\therefore \frac{\rho u^2}{t c_s^2} \ll \frac{\rho u}{l}$ Assuming $u \sim \frac{l}{t} \Rightarrow t \gg l / c_s \Rightarrow$ Information propagates instantaneously

Parameters of the system:

- characteristic (outer-scale) velocity, u_0
- characteristic (outer-scale) length, L
- viscosity, ν set by molecular properties

* Outer-scale is also called the integral or autocorrelation scale
Let's compare 2 important terms in the NS eqn
 $L^{int} = \int_0^\infty R_{ii}(r,t) dr$; $R_{ii} = \frac{\langle u_i(x_i,t) u_i(x_i+t,t) \rangle}{\langle u_i^2 \rangle}$

$\frac{\text{convection}}{\text{viscous}} \sim \frac{u_0^2 / L}{\nu u_0 / L^2} = \frac{u_0 L}{\nu} \equiv Re$ Reynolds number

- When Re is "small", viscous effects dominate and the flow is linear (laminar)
- When Re is sufficiently large, the flow becomes chaotic \rightarrow turbulent. How large is large enough depends on the system, but values of $10^2 - 10^4$ are typical.
- The transition between laminar and fully developed turbulence is very messy, so we will focus on fully developed turbulence only.

Phenomenological picture of turbulence

- At each point in the fluid, the velocity is fluctuating around its mean value \vec{u}_0

$$\vec{u} = \vec{u}_0 + \delta\vec{u}$$

At the outer-scale, $\delta u_0 \sim \delta u_L$. Also, we can transform away the mean flow. So, we can redefine Re in terms of fluctuating quantities

$$Re = \frac{\delta u_L L}{\nu}$$

- Let us now consider what happens to the energy in this system $E = \frac{1}{2} \int d\vec{x} |\vec{u}|^2$

Dotting the NS eqn with $\vec{u} \Rightarrow$

$$\frac{dE}{dt} = \underbrace{\nu \int d\vec{x} \vec{u} \cdot \nabla^2 \vec{u}}_{\text{viscous dissipation}} + \underbrace{\int d\vec{x} \vec{u} \cdot \vec{f}}_{\text{rate of energy injection}}$$

If our system is in a stationary state

(formally, we are considering the ensemble average $\equiv \langle \rangle$)

then

$$\frac{d\langle E \rangle}{dt} = 0 = \nu \int d\vec{x} \langle \vec{u} \cdot \nabla^2 \vec{u} \rangle + \underbrace{\int d\vec{x} \langle \vec{u} \cdot \vec{f} \rangle}_{\substack{=: \int_V E \\ \text{volume}}}$$

$$\therefore -\nu \int d\vec{x} \langle \vec{u} \cdot \nabla^2 \vec{u} \rangle = \int_V E$$

In a steady state, the energy input rate, E , must match the dissipation rate.

- Let's now construct estimates for various quantities based on dimensional analysis

At the outer-scale, the turbulence is characterized by u_0, L . At smaller scales, we can consider the RMS velocity u_e at scale l . Using just the velocity, length scale, and viscosity we now construct other important quantities

Eddy turnover time: $t_e \sim \frac{l}{u_e}$

at the outer-scale $t_L \sim \frac{L}{u_0}$

- Energy injection rate: $\epsilon \sim \frac{u_0^3}{L} \sim \frac{u_0^2}{t_L}$

Using the energy injection rate, we can re-write

$$t_L \sim \epsilon^{-1/3} L^{2/3} \quad (1)$$

- Dissipation time scale: $t_e^{diss} \sim \frac{l^2}{\nu} \quad (2)$

- Viscous scale: Equating (1) and (2)

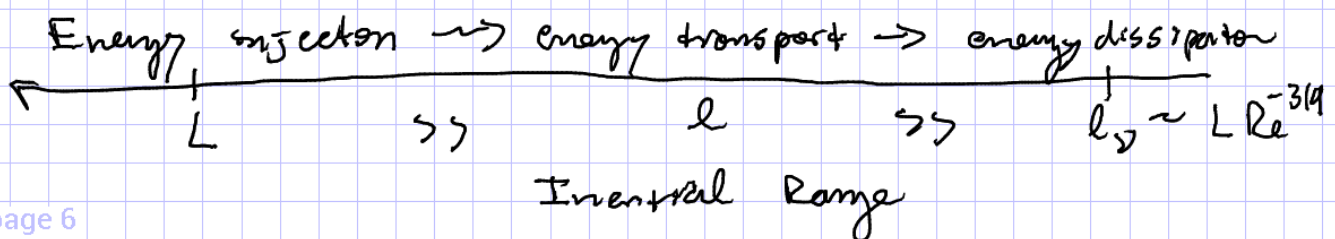
$$\Rightarrow l_\nu \sim \left(\frac{\nu^3}{\epsilon} \right)^{1/4} \sim L Re^{-3/4} \ll L$$

Note that this scale has multiple names:

viscous scale, inner scale, dissipation scale, Kolmogorov scale are all common

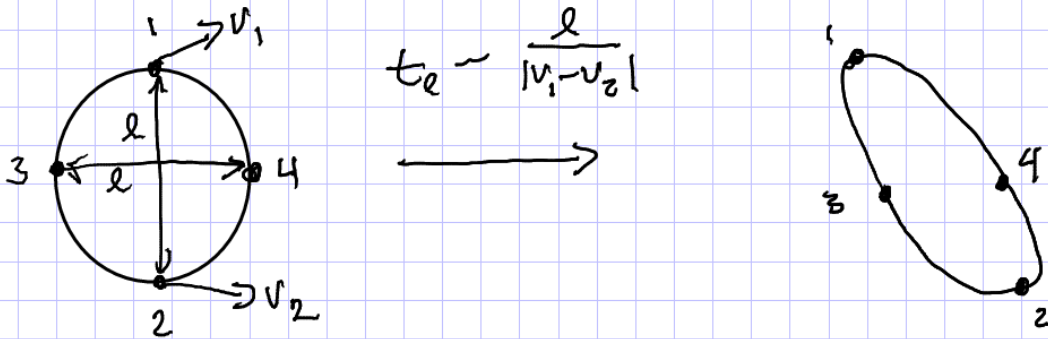
Similarly, the outer-scale is often called the energy containing scale or integral scale

- basic picture at this point



- Let's finish the cartoon picture of turbulence before we move on to K41.

- I defined the eddy turnover time above as $t_e \sim \frac{l}{u_e}$, but what does it mean? t_e is the characteristic time for a structure of size l to undergo a significant distortion due to the relative motion of its components



$\nabla \cdot u = 0 \Rightarrow$ the area is conserved \Rightarrow if 1 & 2 separate, 3 & 4 become closer. $\therefore t_e$ is also the typical time for the transfer of energy from scale l to a smaller scale. Also call this the cascade time.

Kolmogorov 1941 Turbulence theory

Before we discuss the theory, let's establish a baseline.

What observational facts do we know that we can use to constrain theory?

1) **2/3 law** the mean square velocity increments, $\langle \delta u_l^2 \rangle$ between two points separated by l scales as $\langle \delta u_l^2 \rangle \sim l^{2/3}$

2) **Finite energy dissipation** the energy dissipation is always positive and finite

- In 1922, Richardson conjectured that the energy transfer is local in space to the viscous scale



but this conjecture alone does not reproduce the observable aspects of turbulence above

- So, in 1941 Kolmogorov proposed the first theory that did explain 1) & 2) above. To do so, he assumed the following

- 0) Universality: The turbulence, inertial range, is independent of the particular forcing (and dissipation)
- 1) Locality of interactions
- 2) Homogeneity: No special points \Rightarrow no intermittency
- 3) Isotropy: No special directions
- 4) Scale invariance: No special scales \Rightarrow constant cascade rate, ϵ .

\Rightarrow Scale invariance $\Rightarrow \epsilon = \text{const}$, but we already argued that $\epsilon \sim \frac{u_0^3}{L}$, since $\epsilon = \text{const}$,

$$\epsilon \sim \frac{\delta u_l^3}{l} \quad \therefore \quad \delta u_l \sim (\epsilon l)^{1/3} \quad \Rightarrow \quad \delta u_l^2 \sim \epsilon^{2/3} l^{2/3}$$

and we have the $2/3$ law!

$\delta u_l \sim (\epsilon l)^{1/3}$ is referred to as the Kolmogorov - Obukhov law

• Energy spectra

In general, $\vec{k} = (k_x, k_y, k_z)$, so $E^{(3)}(\vec{k})$ is the 3D energy spectrum. The total energy is thus $E = \int d\vec{k} E^{(3)}(\vec{k})$. If the energy is isotropic in k space ($|k| \gg \lambda$), then we can use spherical coordinates

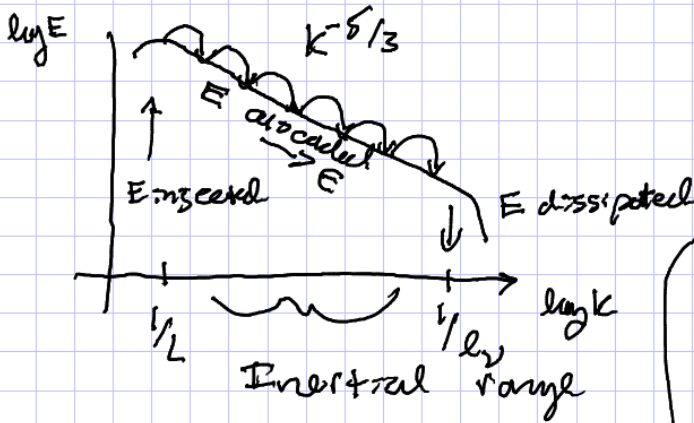
$$E = \iiint dk d\theta d\phi k^2 \sin\theta E^{(3)}(\vec{k}) = \int dk k^2 E^{(3)}(k) = \int dk E^{(1)}(k)$$

Where $E^{(1)}(k)$ is the 1D energy spectrum.

$$\therefore E = \int u_e^2 \sim E^{2/3} l^{2/3} \sim E^{2/3} k^{-2/3} \sim \int_{k=1/l}^{\infty} dk k^2 E^{(3)} = \int dk E^{(1)}(k)$$

$$\Rightarrow \underline{E^{(1)} \sim E^{2/3} k^{-5/3}} \quad \text{and} \quad E^{(3)} \sim E^{2/3} k^{-11/3}$$

Normally use the 1D spectrum



What about scales $l < \lambda_v$ and $l > L$?

1) $l > L$: $E = u_0^2 = \text{const} \Rightarrow E^{(1)} \sim k^{-1}$

2) $l < \lambda_v$: $E \sim \nu \vec{u} \cdot \nabla^2 \vec{u} \sim \nu \frac{\delta u_0^2}{l^2} \Rightarrow \int u_e^2 \sim \left(\frac{E}{\nu}\right)^{1/2} l \Rightarrow E^{(1)} \sim k^{-3}$

Inertial range is the range of scales unaffected by driving or dissipation. The physics is assumed to be self-similar (fractal) here.

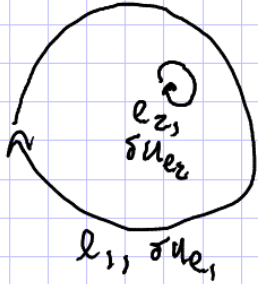
Note that $E \sim l^{2/3}$ dominated by large scales and gradients $\frac{\delta u_0}{l} \sim l^{-2/3}$ dominated by small scales \Rightarrow viscous cutoff.

Also, the cascade time, $t_c \sim \frac{l}{\delta u_e} \sim l^{2/3}$ decreases with scale.

'Verify' that the cascade is local

Consider motions at scales l_1 and l_2 .

1) Can large scale motion shear apart small scales before they cascade?



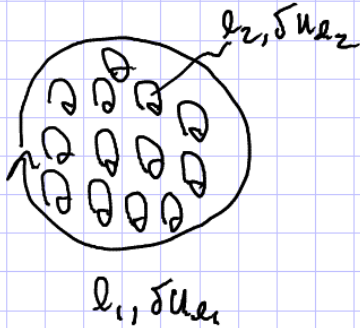
shearing time $= t_s \sim \frac{l_1}{\delta u_{l_1}}$

cascade time for l_2 $t_{c2} \sim \frac{l_2}{\delta u_{l_2}}$

$$\frac{t_s}{t_{c2}} \sim \frac{l_1 \delta u_{l_2}}{l_2 \delta u_{l_1}} \sim \frac{l_1 \left[\delta u_{l_1} \left(\frac{l_2}{l_1} \right)^{1/3} \right]}{l_2 \delta u_{l_1}}$$

$\sim \left(\frac{l_1}{l_2} \right)^{2/3} \gg 1 \Rightarrow$ shearing by large scales not important.

2) Can small scale eddies diffuse the large eddies before they cascade?



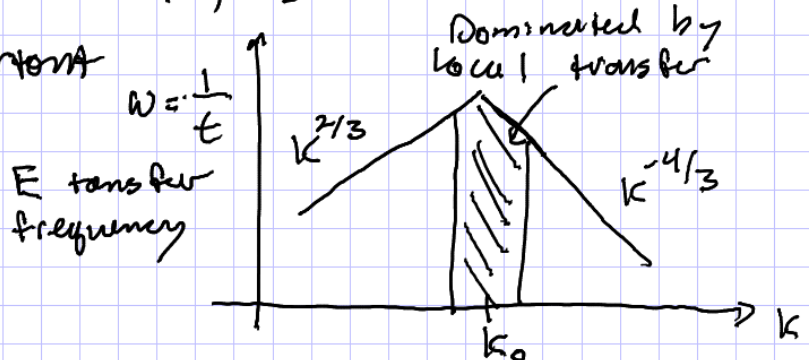
Diffusion coefficient due to eddies of size l_2 : $D = \frac{l_2^2}{t_{c2}} = l_2 \delta u_{l_2}$

Time to diffuse distance l_1 is

$$t_D \sim \frac{l_1^2}{D} \sim \frac{l_1^2}{l_2 \delta u_{l_2}}$$

$$\frac{t_D}{t_{c1}} \sim \frac{l_1^2 \delta u_{l_1}}{l_2 \delta u_{l_2}} \sim \frac{l_1 \delta u_{l_1}}{l_2 \left[\delta u_{l_1} \left(\frac{l_2}{l_1} \right)^{1/3} \right]} = \left(\frac{l_1}{l_2} \right)^{4/3} \gg 1 \Rightarrow$$

diffusion is unimportant



Additional Reading

- 1) Uwe Frisch "Turbulence: The Legacy of A.N. Kolmogorov" 1996
- 2) Landau B Lifshitz "Fluid Mechanics" 1987
chapter 3
- 3) Kolmogorov 1941. Translation by Lewis 1951
"The local structure of turbulence in incompressible
viscous fluid for very large Reynolds numbers"
- 4) P.A. Davidson "Turbulence: An Introduction" 2004